# Polymerization of Ethylene by Zirconocene-B $\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ Catalysts with Aluminum Compounds 

SHENGSHENG LIU, GUANGQIAN YU, BAOTONG HUANG<br>Changchun Institute of Applied Chemistry, Chinese Academy of Sciences, Changchun, 130022, People's Republic of China

Received 30 January 1997; accepted 25 March 1997


#### Abstract

Ethylene polymerization by zirconocene- $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ catalysts with various aluminum compounds has been investigated. It is found that the catalytic activity depended on zirconocenes used, and especially on the type of aluminum compounds. For $\mathrm{Et}\left(\mathrm{H}_{4} \mathrm{Ind}\right)_{2} \mathrm{ZrCl}_{2}\left(\mathrm{H}_{4}\right.$ Ind : tetrahydroindenyl), the activity decreases in the following order: $\mathrm{Me}_{3} \mathrm{Al}>i-\mathrm{Bu}_{3} \mathrm{Al}>\mathrm{Et}_{3} \mathrm{Al}>\mathrm{Et}_{2} \mathrm{AlCl}$. While for $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}(\mathrm{Cp}$ : cyclopentadienyl), it varies as follows: $i$ - $\mathrm{Bu}_{3} \mathrm{Al}>\mathrm{Me}_{3} \mathrm{Al}>\mathrm{Et}_{3} \mathrm{Al}$. Furthermore, the activity is significantly affected by the addition mode of the catalytic components, which may imply that the formation of active centers is associated with an existing concentration of catalytic components. Results of thermal behavior of polyethylene (PE) studied by differential scanning calorimetry (DSC) show that crystallinity of the polymer prepared with $\mathrm{Et}_{3} \mathrm{Al}$ is higher than that with $\mathrm{Me}_{3} \mathrm{Al}$ or $i-\mathrm{Bu}_{3} \mathrm{Al}$. It is also found that the numberaverage molecular weight $(\bar{M})$ of the polymers prepared with $\mathrm{Me}_{3} \mathrm{Al}$ or $i-\mathrm{Bu}_{3} \mathrm{Al}$ is much higher than that with $\mathrm{Et}_{3} \mathrm{Al} .{ }^{1} \mathrm{H}$-NMR studies substantiate that $i$ - $\mathrm{Bu} u_{3} \mathrm{Al}$ is a more efficient alkylation agent of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ in comparison with $\mathrm{Me}_{3} \mathrm{Al}$. © 1997 John Wiley \& Sons, Inc. J Appl Polym Sci 66: 1715-1720, 1997


Key words: ethylene; polymerization; zirconocene; aluminium compound; ${ }^{1} \mathrm{H}-\mathrm{NMR}$

## INTRODUCTION

The homogeneous Ziegler-Natta catalyst $\mathrm{Cp}_{2} \mathrm{TiCl}_{2}-$ $\mathrm{R}_{2} \mathrm{AlCl}$, first described by Breslow and Newburg, ${ }^{1,2}$ has low activity for ethylene polymerization because of bimolecular deactivation due to reductive metathesis. Kaminsky and Sinn obtained an extremely active catalyst by substituting Zr for Ti and using methylaluminoxane (MAO) as cocatalyst. ${ }^{3}$ Furthermore, Kaminsky et al. ${ }^{4}$ found that $r a c-E t(\text { Ind })_{2} \mathrm{ZrCl}_{2}-\mathrm{MAO}\left[\mathrm{Et}(\text { Ind })_{2}\right.$ = ethylene-bis(indenyl)] can catalyze stereospecific polymerization of $\alpha$-olefin in soluble systems. Metallocene catalysts that provide

[^0]access to, besides isotactic, ${ }^{5,6}$ isotactic-stereoblock, ${ }^{7}$ syndiotactic, ${ }^{8}$ and isotactic-atactic, block ${ }^{9}$ polypropylenes have been developed. Unfortunately, these catalysts require a large amount of MAO to realize the maximum catalytic activity, which, on some extent, may impair its value in commercial applications. In view of this, much effort has been made not only to lower the amount of MAO in polymerization but also to find a new cocatalyst in place of MAO.

One way of lowering the amount of MAO is to immobilize the zirconocene on a support, such as $\mathrm{SiO}_{2}, \mathrm{Al}_{2} \mathrm{O}_{3}$, or other supports of high surface area. ${ }^{10-16}$ In several cases, it is claimed that additional MAO is not needed during polymerization if it is initially deposited on the surface during preparation of the supported catalyst. Since many polyolefin manufacturing plants are based on fluidized bed technology, the supported metallocene

Table I Ethylene Polymerization with $\mathbf{E t}\left(\mathbf{H}_{4} \mathbf{I n d}\right)_{2} \mathbf{Z r C l}_{2}-\mathbf{B}\left(\mathbf{C}_{6} \mathbf{F}_{5}\right)_{3}-\mathbf{R}_{3} \mathrm{Al}$

| No. | $\mathrm{R}_{3} \mathrm{Al}$ (mmol) |  | Activity $\left(10^{6} \mathrm{~g} \mathrm{~mol} \mathrm{Zr}\right)$ | Crystallinity (\%) | $\begin{gathered} T_{m} \\ \left({ }^{\circ} \mathrm{C}\right) \end{gathered}$ | $\bar{M}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 1 | $\mathrm{Me}_{3} \mathrm{Al}$ | 0.20 | 1.20 | 58.8 | 138.8 | $1.59 \times 10^{5}$ |
| 2 | $\mathrm{Me}_{3} \mathrm{Al}$ | 0.45 | 1.61 | - | - | - |
| 3 | $\mathrm{Me}_{3} \mathrm{Al}$ | 0.60 | 1.82 | - | - | - |
| 4 | $\mathrm{Me}_{3} \mathrm{Al}$ | 1.00 | 1.48 | - | - | - |
| 5 | $\mathrm{Et}_{3} \mathrm{Al}$ | 0.40 | 0.62 | - | - | - |
| 6 | $\mathrm{Et}_{3} \mathrm{Al}$ | 0.80 | 0.50 | 74.5 | 135.2 | $0.35 \times 10^{5}$ |
| 7 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 0.40 | 1.25 | 57.3 | 136.7 | $2.15 \times 10^{5}$ |
| 8 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 0.60 | 1.01 | - | - | $1.48 \times 10^{5}$ |
| 9 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 1.00 | 0.85 | - | - | - |
| 10 | $\mathrm{EtAlCl}_{2}$ | 1.00 | trace | - | - | - |
| 11 | MAO | 3.00 | 3.18 | - | 134.4 | $1.08 \times 10^{5}$ |

Conditions: $\mathrm{Et}\left(\mathrm{H}_{4} \mathrm{Ind}\right)_{2} \mathrm{ZrCl}_{2}, 2 \mu \mathrm{~mol} ; \mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}, 3 \mu \mathrm{~mol}$; toluene, 100 mL ; ethylene pressure, $0.4 \mathrm{~atm} ; 50^{\circ} \mathrm{C}$, 30 min . Order of addition of catalysts: $\mathrm{R}_{3} \mathrm{Al}$; $\mathrm{Et}\left(\mathrm{H}_{4} \mathrm{Ind}\right)_{2} \mathrm{ZrCl}_{2} ; \mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$.
catalysts would add new dimensions to their usefulness.

On the other hand, satisfactory results have been obtained by using new activators in the place of MAO, such as $\left[\mathrm{C}_{6} \mathrm{H}_{5}\left(\mathrm{CH}_{3}\right)_{2} \mathrm{NH}^{+}\right]\left[{ }^{-} \mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{4}\right]$, $\left[\left(\mathrm{C}_{6} \mathrm{H}_{5}\right)_{3} \mathrm{C}^{+}\right]\left[{ }^{-} \mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{4}\right]$, and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3} .{ }^{17-19} \mathrm{~A}$ significant advantage is that only a stoichiometric amount of the cocatalyst is required to achieve the maximum catalytic activity of the system.

This article reports the results of ethylene polymerization by zirconocene- $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ catalyst with different aluminum compounds, such as $\mathrm{Me}_{3} \mathrm{Al}, \mathrm{Et}_{3} \mathrm{Al}, i-\mathrm{Bu}_{3} \mathrm{Al}$, etc. The properties of polyethylene (PE) prepared with the above catalytic systems have been characterized. The interaction between $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}, \mathrm{~B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$, and $\mathrm{R}_{3} \mathrm{Al}$ was studied by ${ }^{1} \mathrm{H}-\mathrm{NMR}$ spectroscopy.

## EXPERIMENTAL

## Materials

Ethylene, polymerization-grade from Liaoyang Chemical Corporation, was used without further treatment. Toluene as the solvent was dried with 4A molecular sieves, then distilled in the presence of $\mathrm{Na}-\mathrm{K}$ alloy. $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}, \mathrm{Et}\left(\mathrm{H}_{4} \mathrm{Ind}\right)_{2} \mathrm{ZrCl}_{2}$, and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ were of commercial origin (Boulder Scientific Company, Mead). $\mathrm{Me}_{3} \mathrm{Al}, \mathrm{Et}_{3} \mathrm{Al}, i-\mathrm{Bu}_{3} \mathrm{Al}$, and $\mathrm{Et}_{2} \mathrm{AlCl}$ (Fluka AG, Buchs) were used as received.

## Polymerization

Polymerization of ethylene was carried out with stirring in a 250 mL glass reactor under an atmosphere of argon. After evacuating the reactor for 1 $h$, it was filled with purified argon to atmospheric pressure, and toluene was injected into the reactor; and the monomer, aluminum compound, zirconocene, and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ were added separately in that order. After a specified polymerization time, an ethanol solution of hydrochloric acid was injected into the reactor to quench the polymerization. The polymer was washed several times with ethanol and dried under vacuum at $50^{\circ} \mathrm{C}$ for two days.

## Characterization

Differential scanning calorimetry (DSC) measurements were made with a Perkin-Elmer DSC7 system. Each sample was heated from 40 to $100^{\circ} \mathrm{C}$ at a heating rate of $10^{\circ} \mathrm{C}$ min and kept at this temperature for 5 min . It was then cooled to $40^{\circ} \mathrm{C}$ at a rate of $10^{\circ} \mathrm{C} \mathrm{min}$ and reheated at the same rate. The values of melting point ( $T_{m}$ ) were obtained in the second scan. Crystallinity of the polymers was calculated from the equation

$$
\chi(\%)=\left(\Delta H_{m} / \Delta H_{m}^{\circ}\right) \times 100
$$

where $\Delta H_{m}$ is the heat of fusion of the samples, as determined from the DSC curves of the second heating process, and $\Delta H_{m}{ }^{\circ}$ is the heat of fusion of perfectly crystalline polyethylene, 286 J g . ${ }^{20}$


Figure 1 DSC curves of PE prepared with the $\mathrm{Et}\left(\mathrm{H}_{4} \mathrm{Ind}\right)_{2} \mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-\mathrm{Et}_{3} \mathrm{Al}$ catalyst: (a) the first heating process; (b) the second heating process.

The number-average molecular weight ( $\bar{M}$ ) of the polymers were determined from the following equation ${ }^{21}$ :

$$
[\eta]=2.30 \times 10^{-4} \bar{M}^{0.82}
$$

where [ $\eta$ ] denotes the intrinsic viscosity of the polymer solution obtained with an Ubbelohde viscometer in decalin at $135^{\circ} \mathrm{C}$ according to the usual procedure.
${ }^{1} \mathrm{H}$-NMR analyses of the reactions between $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-\mathrm{R}_{3} \mathrm{Al}$ were performed at room temperature with a Varian NMR-400 spectrometer operating in Fourier transform mode. The benzene $-\mathrm{d}_{6}$ ( $99 \%$, Aldrich) used as solvent was dried over calcium hydride for several days, followed by distillation. The chemical shift of benzene protons as internal standard is $\delta=7.27 \mathrm{ppm}$. About $6 \mathrm{mg}(20 \mu \mathrm{~mol})$ of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ were dissolved
in 0.5 mL of benzene $-\mathrm{d}_{6}$, then aluminum compounds and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ were introduced to the nuclear magnetic resonance (NMR) tube.

## RESULTS AND DISCUSSION

## Polymerization with Et $\left(\mathrm{H}_{4} \operatorname{Ind}\right)_{2} \mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-$ $R_{3}$ Al System

According to the generally accepted point of view, zirconocenium species can be produced by the reaction of dimethyl zirconocene derivative with $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$. For dichlorozirconocene, it needs to be alkylated first, followed by extraction of the anionic ligand to produce the active species.

Despite several papers on zirconocene- $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ catalyst in ethylene or propylene polymerization, ${ }^{22-24}$ the effect of aluminum compounds on these polymerizations seems to be scarce. In the present work, different aluminum compounds are employed to alkylate dichlorozirconocene. The results of ethylene polymerization with $\mathrm{Et}\left(\mathrm{H}_{4} \operatorname{Ind}\right)_{2^{-}}$ $\mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-\mathrm{R}_{3} \mathrm{Al}$ were summarized in Table I.

It can be seen from Table I that aluminum compounds are so important that they can cause up to a more than a three-fold difference in polymerization activity under otherwise identical conditions. Activities of the aluminum compounds decrease in the following order: $\mathrm{Me}_{3} \mathrm{Al}>i-\mathrm{Bu}_{3} \mathrm{Al}$ $>\mathrm{Et}_{3} \mathrm{Al}>\mathrm{EtAlCl}_{2}$. The much lower activity achieved by $\mathrm{Et}_{2} \mathrm{AlCl}$ may be attributed to the fact that $\mathrm{Et}_{2} \mathrm{AlCl}$ cannot effectively alkylate dichloro-

Table II Ethylene Polymerization with $\mathbf{C p}_{2} \mathbf{Z r C l}_{2}-\mathbf{B}\left(\mathbf{C}_{6} \mathbf{F}_{5}\right)_{3}-\mathbf{R}_{3} \mathrm{Al}$ System

| No. | $\mathrm{R}_{3} \mathrm{Al}$ | $(\mathrm{mmol})$ | Activity <br> $\left(10^{6} \mathrm{~g} \mathrm{~mol} \mathrm{Zr}\right)$ |
| :---: | :---: | :---: | :---: |
| 12 | $\mathrm{Me}_{3} \mathrm{Al}$ | 1.0 | 0.05 |
| 13 | $\mathrm{Me}_{3} \mathrm{Al}$ | 2.0 | 0.03 |
| 14 | $\mathrm{Et}_{3} \mathrm{Al}$ | 0.6 | trace |
| 15 | $\mathrm{Et}_{3} \mathrm{Al}$ | 2.0 | trace |
| 16 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 0.2 | trace |
| 17 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 0.4 | 0.52 |
| 18 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 0.6 | 0.82 |
| 19 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 0.8 | 1.35 |
| 20 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 1.0 | 1.10 |
| 21 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 1.5 | 0.68 |
| 22 | $i-\mathrm{Bu}_{3} \mathrm{Al}$ | 2.0 | 0.30 |

Table III Effect of Mode of Catalyst Addition on Ethylene Polymerization

|  | $i-\mathrm{Bu}_{3} \mathrm{Al}(\mathrm{mmol})$ |  |  |  |
| :--- | :---: | :---: | :---: | :---: |
| No. | To Reactor | From Ampoule |  | Activity <br> $\left(10^{6} \mathrm{~g} \mathrm{~mol} \mathrm{Zr}\right)$ |
| 23 | 0.2 | 0.1 | 0.3 | 1.10 |
| 24 | 0.2 | 0.2 | 0.4 | 2.65 |
| 25 | 0.2 | 0.3 | 0.5 | 1.55 |
| 26 | 0.2 | 0.4 | 0.6 | 1.15 |
| 27 | 1.3 | 0.2 | 1.5 | trace |
| 28 | 1.5 | 0.2 | 1.7 | trace |

Conditions: $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}, 2 \mu \mathrm{~mol}$; others as in Table I.
zirconocene due to its relatively low content of alkyl groups in $\mathrm{Et}_{2} \mathrm{AlCl}$.

The effect of concentration of aluminum compounds on activity is evident. For $\mathrm{Me}_{3} \mathrm{Al}$, polymerization activity increased with increments of $\mathrm{Me}_{3} \mathrm{Al}$ from 0.2 to 0.6 mmol ; however, it decreased slightly, with a further increase in concentration. The same results were obtained when using $i$ $\mathrm{Bu}_{3} \mathrm{Al}$ as the cocatalyst in place of $\mathrm{Me}_{3} \mathrm{Al}$.

It is well known that the melting point ( $T_{m}$ ) of PE is lowered after reheating to erase the thermal history. ${ }^{25}$ For the polymer prepared with $\mathrm{Et}_{3} \mathrm{Al}$ in this work, however, the $T_{m}$ value from the second heating process is higher than that from the first one (Fig. 1), the reason for which is not explicit.

Comparing the data in Table I, one can see that:
(1) The polymers obtained with $\mathrm{Me}_{3} \mathrm{Al}$ or $i$ $\mathrm{Bu}_{3} \mathrm{Al}$ have much higher number-average molecular weight ( $\bar{M}=1.48-2.15 \times 10^{5}$ ) than that with $\mathrm{Et}_{3} \mathrm{Al}\left(\bar{M}=0.35 \times 10^{5}\right)$, which may imply that the polymer chain transfer to $\mathrm{Et}_{3} \mathrm{Al}$ is easier than to $\mathrm{Me}_{3} \mathrm{Al}$ or $i-\mathrm{Bu}_{3} \mathrm{Al}$.
(2) Using MAO in place of $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3} / i-\mathrm{Bu}_{3} \mathrm{Al}$ ( or $\mathrm{Me}_{3} \mathrm{Al}$ ), the polymer has a lower $\bar{M}$.
(3) Crystallinity of polymers obtained with $\mathrm{Et}_{3} \mathrm{Al}$ is higher than that with $i-\mathrm{Bu}_{3} \mathrm{Al}$ or $\mathrm{Me}_{3} \mathrm{Al}$.

## Polymerization with $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-\mathrm{R}_{3} \mathrm{Al}$ System

Results of ethylene polymerization with $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ / $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3} / \mathrm{R}_{3} \mathrm{Al}$ system are tabulated in Table II.

The effect of aluminum compounds on polymerization is evident (Table II). For $i$ - $\mathrm{Bu}_{3} \mathrm{Al}$, the activity increased monotonously with $\left[i-\mathrm{Bu}_{3} \mathrm{Al}\right]$ un-
til it reached $0.8 \mathrm{mmol}\left(1.35 \times 10^{6} \mathrm{~g} \mathrm{~mol} \mathrm{Zr}\right)$ and then decreased rapidly on further increase in $i$ $\mathrm{Bu}_{3} \mathrm{Al}$ until it reached only $0.30 \times 10^{6} \mathrm{~g} \mathrm{~mol} \mathrm{Zr}$ at $\left[i-\mathrm{Bu}_{3}^{-} \mathrm{Al}\right]$ of 2.0 mmol . It is deduced that the surplus $i-\mathrm{Bu}_{3} \mathrm{Al}$ may lead to the formation of species like $\left[\mathrm{Cp}_{2} \mathrm{ZrR}^{+}\right]\left[{ }^{-} \mathrm{Cl}_{2} \mathrm{AlR}_{2}\right]$, preventing further reaction between the alkylated zirconiocene and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$. As we know, the species $\left[\mathrm{Cp}_{2} \mathrm{ZrR}^{+}\right]\left[{ }^{-} \mathrm{ClB}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}\right]^{23}$ is highly active, whereas the species as $\left[\mathrm{Cp}_{2} \mathrm{ZrR}^{+}\right]\left[{ }^{-} \mathrm{Cl}_{2} \mathrm{AlR}_{2}\right]$ are much less active, which probably explains the lowering in activity when $i-\mathrm{Bu}_{3} \mathrm{Al}$ exceeds a certain amount.

Use of $\mathrm{Et}_{3} \mathrm{Al}$ and $\mathrm{Me}_{3} \mathrm{Al}$ in place of $i$ - $\mathrm{Bu}_{3} \mathrm{Al}$ gives rise to reduction in activity. The activities of various aluminum compounds used as cocatalyst decrease in the following order: $i-\mathrm{Bu}_{3} \mathrm{Al}>\mathrm{Me}_{3} \mathrm{Al}$ $\Rightarrow \mathrm{Et}_{3} \mathrm{Al}$.

Change in mode of addition of catalytic components was performed as follows. Only part of the $i-\mathrm{Bu}_{3} \mathrm{Al}(0.2 \mathrm{mmol})$ was first added to the reactor, and the rest of the $i-\mathrm{Bu}_{3} \mathrm{Al}$ and the whole of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ were introduced to a 40 mL ampoule containing 20 mL toluene, which were then injected into the polymerization reactor. It is found that, as shown in Table III, the polymerization behavior is dramatically altered.

For experiments 23-26, the activities are relatively higher at total amounts of $i-\mathrm{Bu}_{3} \mathrm{Al}$, as shown in Table II. When the total amount of $i$ $\mathrm{Bu}_{3} \mathrm{Al}$ reaches 0.4 mmol , the activity is $2.65 \times 10^{6}$ g mol Zr , a five-fold increase as compared to No. 13 in Table II.

Keeping the catalytic components in the ampoules unchanged, extremely low activities were obtained with further increment of $i-\mathrm{Bu}_{3} \mathrm{Al}$ in the polymerization reactor (Nos. 27, 28). It is inferred that the highly active species of $\left[\mathrm{Cp}_{2} \mathrm{ZrR}^{+}\right]-$ $\left[{ }^{-} \mathrm{ClB}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}\right]$ produced in the ampoule is de-


Figure $2{ }^{1} \mathrm{H}$-NMR spectra of the catalytic components $\left(\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}\right.$ is abbreviated as B$)$ : (a) $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-$ $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}(\mathrm{~B}-\mathrm{Zr}=1)$; (b) $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-i-\mathrm{Bu}_{3} \mathrm{Al}(\mathrm{Al}-\mathrm{Zr}$ $=1)$; (c) (b) $-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}(\mathrm{~B}-\mathrm{Zr}=1)$; (d) $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-$ $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-i-\mathrm{Bu}_{3} \mathrm{Al}(\mathrm{Al}-\mathrm{Zr}=5 ; \mathrm{B}-\mathrm{Zr}=1)$.
stroyed by the excess $i-\mathrm{Bu}_{3} \mathrm{Al}$ in the reactor, and the formation of active centers results at a required concentration of the catalytic components. The reversible reaction between different active species may be represented as
$\left[\mathrm{Cp}_{2} \mathrm{ZrR}^{+}\right]\left[-\mathrm{ClB}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}\right] \underset{-\mathrm{R}_{3} \mathrm{Al}}{\stackrel{+\mathrm{R}_{3} \mathrm{Al}}{\rightleftharpoons}}$

$$
\left[\mathrm{Cp}_{2} \mathrm{ZrR}^{+}\right]\left[\left[^{-} \mathrm{ClAlR}_{3}\right]+\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}\right.
$$

Compared with the usual addition procedure, a change in the mode of addition of the catalysts with limited amount of total $i-\mathrm{Bu}_{3} \mathrm{Al}$ leads to much higher activity, which is significant for commercial utilization.

## ${ }^{1}$ H-NMR Analyses of the Catalysts

The reaction between $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}, \mathrm{~B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$, and $\mathrm{R}_{3} \mathrm{Al}$ in benzene- $\mathrm{d}_{6}$ at room temperature was monitored by means of ${ }^{1} \mathrm{H}-\mathrm{NMR}$ spectroscopy. Dissolution of solid $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}(20 \mu \mathrm{~mol})$ in a solution of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}(20 \mu \mathrm{~mol})$ gave no new signals, except that at $\delta=5.86 \mathrm{ppm}$, assigned to be due to cyclopentadienyl of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ [Fig. 2(a)]. It is inferred that no interaction between $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ and $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ occurred. For $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-i-\mathrm{Bu}_{3} \mathrm{Al}(\mathrm{Al}-\mathrm{Zr}$ $=1$ ), a signal appeared at $\delta=5.724 \mathrm{ppm}$, assigned to be due to cyclopendienyl of $\mathrm{Cp}_{2} \mathrm{Zr}(i$ $\mathrm{Bu}) \mathrm{Cl}$ [Fig. 2(b)]. The alkylation reaction between $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ and $i$ - $\mathrm{Bu}_{3} \mathrm{Al}$ is almost complete in


Figure $3{ }^{1} \mathrm{H}$-NMR spectra of the $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-$ $\mathrm{Me}_{3} \mathrm{Al}$ system $(\mathrm{B}-\mathrm{Zr}=1)$ : (a) $\mathrm{Al}-\mathrm{Zr}=5$; (b) $\mathrm{Al}-\mathrm{Zr}=$ 20.
the case of $\mathrm{Al}-\mathrm{Zr}=1$. Addition of $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}(\mathrm{~B}-$ $\mathrm{Zr}=1$ ) to the solution of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-i-\mathrm{Bu}_{3} \mathrm{Al}$ led to the appearance of two signals at $\delta=5.641$ and 5.585 ppm , respectively [Fig. 2(c)], substantiating the reaction between $\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}$ and $\mathrm{Cp}_{2} \mathrm{Zr}(i$ $\mathrm{Bu}) \mathrm{Cl}$. The spectrum of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-i$ $\mathrm{Bu}_{3} \mathrm{Al}$ [Fig. 2(d)] on direct addition of the three components to the NMR tube $(\mathrm{Al}-\mathrm{Zr}=5)$ is almost the same as in Fig. 1(c).

The spectrum of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-\mathrm{Me}_{3} \mathrm{Al}$ system is shown in Figure 3. If one divides the signals into two parts, that from the alkylated complex and that from the nonalkylated complex, the alkylation reaction is calculated by integration to be approximately $34 \%$ complete at an $\mathrm{Al}-$ Zr ratio of 5 [Fig. 3(a)]. At a higher $\mathrm{Al}-\mathrm{Zr}$ ratio of 20 , the signals assigned to cyclopentadienyl of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ become complicated, and the conversion is approximately $60 \%$. The conclusion reached is that $i-\mathrm{Bu}_{3} \mathrm{Al}$ is a more effective alkylating agent of $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}$ than $\mathrm{Me}_{3} \mathrm{Al}$. Since the ternary system $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-\mathrm{B}\left(\mathrm{C}_{6} \mathrm{~F}_{5}\right)_{3}-\mathrm{R}_{3} \mathrm{Al}$ is more complex than the binary system $\mathrm{Cp}_{2} \mathrm{ZrCl}_{2}-\mathrm{MAO}$ or $\mathrm{Cp}_{2} \mathrm{ZrR}_{2}-$ $B\left(C_{6} F_{5}\right)_{3}$, further study is in progress and will be reported later.

## REFERENCES

1. D. S. Breslow and N. R. Newburg, J. Am. Chem. Soc., 79, 5073 (1957).
2. D. S. Breslow and N. R. Newburg, J. Am. Chem. Soc., 81, (1959).
3. H. Sinn, W. Kaminsky, H.-J. Vollmer, and R. Woldt, Angew. Chem. Int. Ed. Engl., 19, 390 (1980).
4. W. Kaminsky, K. Kulper, H. H. Brintzinger, and
F. R. W. P. Wild, Angew. Chem. Int. Ed. Engl., 24, 507 (1985).
5. J. A. Ewen, L. Haspeslagh, J. L. Atwood, and H. Zhang, J. Am. Chem. Soc., 109, 6544 (1987).
6. J. A. Ewen, in Catalytic Polymerization of Olefin, T. Keii and K. Soga, Eds., Elsevier, New York, 1986, p. 271.
7. J. A. Ewen, J. Am. Chem. Soc., 106, 6355 (1984).
8. J. A. Ewen, R. L. Jones, A. Razavi, and J. D. Ferrara, J. Am. Chem. Soc., 110, 6255 (1988).
9. D. T. Mallin, M. D. Rausch, Y. Lin, S. Dong, and J. C. W. Chien, J. Am. Chem. Soc., 112, 2030 (1990).
10. J. C. W. Chien and D. He, J. Polym. Sci., Polym. Chem., 29, 1603 (1991).
11. S. Collins, W. M. Kelly, and D. A. Holden, Macromolecules, 25, 1780 (1992).
12. W. Kaminsky and F. Renner, Makromol. Chem., Rapid Commun., 14, 239 (1993).
13. K. Soga and M. Kaminaka, Makromol. Chem., Rapid Commun., 13, 221 (1992).
14. K. Soga and M. Kaminaka, Makromol. Chem. Phys., 195, 1369 (1994).
15. H. C. Welborn, Eur. Pat. 0-334-887 (1989).
16. M. Kloka and N. Kashiwa, Eur. Pat. 0-285-443 (1988).
17. G. G. Hlatky, H. W. Turner, and R. R. Eckman, J. Am. Chem. Soc., 111, 2728 (1989).
18. J. C. W. Chien, W.-M. Tsai, and M. R. Rausch, J. Am. Chem. Soc., 113, 8570 (1991).
19. X. Yang, C. L. Stern, and T. J. Marks, J. Am. Chem. Soc., 113, 3623 (1991).
20. A. P. Gray, Thermochim. Acta 1, 563 (1970).
21. D. G. Boucher, I. W. Parsons, and R. N. Haward, Makromol. Chem., 175, 3641 (1974).
22. J. C. W. Chien and B. P. Wang, J. Polym. Sci., Part A: Polym. Chem., 26, 3089 (1988).
23. J. C. W. Chien, W. Song, and M. D. Rausch, J. Polym. Sci., Part A: Polym. Chem., 32, 2387 (1994).
24. W.-M. Tsai and J. C. W. Chien, J. Polym. Sci., Part A: Polym. Chem., 32, 149 (1994).
25. P. J. Lemstra, Polym. Commun., 32, 343 (1990).

[^0]:    Correspondence to: S. Liu
    Contract grant sponsor: National Natural Science Foundation of China (NNSFC).
    Journal of Applied Polymer Science, Vol. 66, 1715-1720 (1997)
    © 1997 John Wiley \& Sons, Inc.
    CCC 0021-8995/97/091715-06

